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# WGS Catalysis and In Situ Studies of $CoO_{1-x}$, $PtCo_n/Co_3O_4$, and $Pt_mCo_{m'}/CoO_{1-x}$ Nanorod Catalysts

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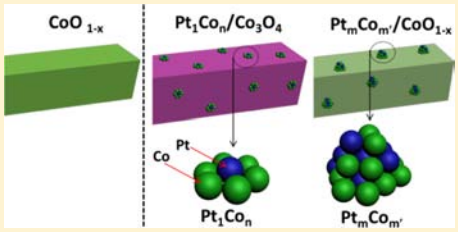
Supporting Information

**ABSTRACT:** Water–gas shift (WGS) reactions on $Co_3O_4$ nanorods and $Co_3O_4$ nanorods anchoring singly dispersed Pt atoms were explored through building correlation of catalytic performance to surface chemistry of catalysts during catalysis using X-ray absorption spectroscopy, ambient pressure X-ray photoelectron spectroscopy (AP-XPS), and environmental TEM. The active phase of pure $Co_3O_4$ during WGS is nonstoichiometric cobalt monoxide with about 20% oxygen vacancies, $CoO_{0.80}$. The apparent activation energy ($E_a$) in the temperature range of 180–240 °C is 91.0 ± 10.5 kJ mol$^{-1}$. $Co_3O_4$ nanorods anchoring Pt atoms ($Pt/Co_3O_4$) are active for WGS with a low $E_a$ of 50.1 ± 5.0 kJ mol$^{-1}$ in the temperature range of 150–200 °C. The active surface of this catalyst is singly dispersed $Pt_1Co_n$ nanoclusters anchored on $Co_3O_4$ ($Pt_1/Co_3O_4$), evidenced by in situ studies of extended X-ray absorption fine structure spectroscopy. In the temperature range of 200–300 °C, catalytic in situ studies suggested the formation of $Pt_mCo_{m'}$ nanoclusters along with the reduction of $Co_3O_4$ substrate to $CoO_{1-x}$. The new catalyst, $Pt_mCo_{m'}/CoO_{1-x}$ is active for WGS with a very low $E_a$ of 24.8 ± 3.1 kJ mol$^{-1}$ in the temperature range of 300–350 °C. The high activity could result from a synergy of $Pt_mCo_{m'}$ nanoclusters and surface oxygen vacancies of $CoO_{1-x}$.




## 1. INTRODUCTION

Water–gas shift (WGS) catalysis with high activity at a temperature near the operational temperature of low-temperature fuel cells is one solution for on-board purification of hydrogen sources for low-temperature fuel cell technology, since the CO tolerance of fuel cell electrodes is only 50 ppm or lower.[1−5] Development of catalysts with high activity at low temperatures has driven significant effort toward fundamental studies of low-temperature WGS on catalysts distinct from industrial Cu and Fe WGS catalysts.[6−8] Noble metals, including Au and Pt impregnated on $CeO_2$ and $TiO_2$, have been extensively studied in recent decades.[9−28] They catalyze WGS through a bifunctional mechanism. Both the metal and oxygen vacancies of reducible oxides play a synergic role in WGS.[18,26,29,30] It is generally acknowledged that metal particles adsorb CO and oxygen vacancies dissociate $H_2O$ molecules to form OH groups. The adsorbed CO molecules couple with the formed OH at the oxide–metal interface, forming an intermediate which reforms and dissociates into $CO_2$ and a hydrogen atom. This hydrogen atom spills over and couples with another hydrogen atom to form a hydrogen molecule.

$Co_3O_4$ is a reducible oxide of an early transition metal. It exhibits extraordinarily high activity in CO oxidation even at −77 °C, due to the weaker bond strength of Co–O and low hopping barrier of oxygen vacancies on the surface, in contrast to most other oxides of the 3d transition metals.[31,32] It has been confirmed that different types of oxygen vacancies play different roles in adsorbing oxygen molecules and dissociating them to provide active oxygen atoms.[33] So far, there has been no conclusive assignment of the active sites and mechanism for CO oxidation on $Co_3O_4$.[33]

Cobalt oxides exist in three different structures, including $Co_3O_4$ with spinel structure, CoO with rocksalt structure, and $Co_2O_3$ with hexagonal structure. $Co_3O_4$ is the thermodynamically favorable phase at room temperature. However, it can be reduced to rocksalt CoO by annealing it in a reducing gas or even just in an ultrahigh high vacuum. In terms of $Co_2O_3$, it is not chemically stable, and thus it is challenging to prepare.[34,35] $Co_3O_4$ exhibits distinctly different packing of the oxygen and cobalt atoms in terms of the crystallographic lattice, in contrast to CoO. Bond lengths of Co(II)–O (1.99 Å) and Co(III)–O (1.89 Å) of $Co_3O_4$[23,36] are slightly shorter than that of the Co(II)–O of CoO (2.13 Å),[37] suggesting a weaker Co–O bond of CoO. The low barrier for the hopping of oxygen vacancies[38] on the $Co_3O_4$ surface shows a high mobility of surface lattice oxygen atoms, making it readily generate oxygen vacancies. It further indicates a higher mobility of oxygen atoms on CoO, in contrast to $Co_3O_4$. Inspired by (1) the role of the oxygen vacancies of the $CeO_2$ and $TiO_2$ surface in WGS on Au

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(or Pt)/$CeO_2$ (or $TiO_2$)[6,7] and (2) the lowest dissociation energy of the M−O bond (M: metal) of cobalt oxides,[10] we hypothesized that cobalt oxide could be a good component for a catalyst in a low-temperature WGS reaction, since it can generate oxygen vacancies readily and its surface lattice oxygen can adsorb CO molecules.[33] As oxygen vacancies can be generated on $Co_3O_4$[31] or CoO under certain conditions, a bifunctional catalyst based on $Co_3O_4$ or CoO could be developed. As the mobility of surface lattice oxygen atoms on cobalt oxide is much larger than that on $TiO_2$ or $CeO_2$,[38] active metals such as Pt could be anchored on $Co_3O_4$ during generation of oxygen vacancies in calcination. Thus, cobalt oxide anchoring Pt atoms could be developed. It could offer different catalytic performances in contrast to Pt/$CeO_2$ and Pt/$TiO_2$ since surface lattice oxygen atoms of $Co_3O_4$ or CoO exhibit high mobility and $Co_3O_4$ could be transformed to $CoO_{1-x}$.

Here we synthesized pure $Co_3O_4$ nanorods and $Co_3O_4$ anchoring Pt atoms. In situ extended X-ray absorption fine structure (EXAFS) measurements established evidence that Pt atoms are dispersed as single atoms on the cobalt oxide support. Their surface chemistry at different temperatures was characterized with ambient pressure XPS (AP-XPS) while a catalyst is placed in a flow reactor installed in AP-XPS. Correlations between catalytic in situ surface chemistry of catalysts during catalysis and their kinetics were built. The as-synthesized $Co_3O_4$ (nominal catalyst) is active for WGS. AP-XPS studies revealed that the active phase of the nominal catalyst, $Co_3O_4$ in WGS, is in fact $CoO_{1-x}$. In situ studies showed that the as-synthesized Pt/$Co_3O_4$ is restructured to $Pt_1Co_n/Co_3O_4$ which is active for WGS in the temperature regime of 150−200 °C with $E_a$ of 50.1 ± 5.0 kJ $mol^{-1}$. $Pt_1Co_n/Co_3O_4$ is further restructured in the temperature range of 200−300 °C, forming a different active phase, $Pt_mCo_{m'}/CoO_{1-x}$. This new phase exhibits high activity at 300−350 °C with an $E_a$ of 24.8 ± 3.1 kJ $mol^{-1}$.

## 2. EXPERIMENTAL SECTION

$Co_3O_4$ nanorods were synthesized with a hydrothermal method. Cobalt acetate tetrahydrate is used as the synthetic precursor. It undergoes a hydrogenolysis process when dissolved in ethylene glycol due to the considerably large molecular ratio of ethylene glycol to water. After the introduction of the sodium carbonate solution, the amount of water molecules increases and triggers hydrolysis along with the attendant fast nucleation of the precursors. The precursors then form layered structures with edge-sharing coordination of hydroxide anions, analogous to the layered double hydroxides, which further form sheet-like structures by self-assembly due to the interlaying hydrogen bonds between the acetates and the hydroxides. Carbonate anions were added to serve as the structure-directing agent. As there are more $Co^{2+}$ in the (110) plane, the recrystallization will be inhibited by the coordination of $Co^{2+}$ to carbonate anions, which gives rise to the preferential exposure of (110) plane. In the aging stage, ethylene glycol is incorporated into the structure by replacing both carbonates and acetates. It largely influences crystalline aggregation and promotes formation of a network of small interconnected pores. Ethylene glycol further contributes to the disintegration of the remaining sheet-like structures and fulfills the formation of pristine nanorods in solution. The pristine nanorods are then washed with deionized water and ethanol and then calcined at 300−450 °C in air for 4 h.

For synthesis of Pt/$Co_3O_4$ catalyst, Pt was anchored on the surface of well crystallized $Co_3O_4$ nanorods with deposition-precipitation.[39] There is no significant change of size and surface morphology in $Co_3O_4$ upon anchoring Pt ions. The Pt/$Co_3O_4$ weight ratio is 0.5% based on the measurements using inductively coupled plasma analysis (ICP) at our Centre for Environmental Science and Technology. The morphology of catalysts was identified with Titan TEM (FEI Titan 80−300, 300 kV FEG TEM with point resolution 0.2 Å). HAADF-STEM images were collected on JEOL JEM-ARM 200F with a CEOS probe corrector in Takeda group at Osaka University at Japan. The used accelerating voltage is 200 kV. The HAADF-STEM resolution is 0.1 nm.

Surface chemistry of the two different nominal catalysts ($Co_3O_4$ or Pt/$Co_3O_4$) before catalysis or any pretreatment was characterized with XPS in ultrahigh vacuum (UHV). Au thin film (0.4-mm thick, 99.99%, VWR) was used as a substrate to load a catalyst. Au foil was deliberately roughened using an SiC knife to increase adhesion. A certain amount of catalyst powder is dispersed into ethanol to prepare an original solution. This solution was further diluted with ethanol to a concentration such that a single layer of nanorods of catalyst ($Co_3O_4$ or Pt/$Co_3O_4$ nanorods) can be prepared by dropping a small droplet of the diluted solution on Au substrate. This concentration can be calculated from the size of $Co_3O_4$ nanorods and the size of Au substrate. Ethanol left in the thin layer on the Au foil is vaporized by placing Au foil in a vacuum oven at 60 °C. A dry Au sample with a layer of physically adsorbed nanorods is ready for XPS studies. Such a preparation of sample for XPS studies can effectively minimize surface charging resulting from thick catalyst layers. The apparent binding energies of Au 4f, Co 2p, and O 1s of sample prepared with the above method are very close to their real values, suggesting there is no obvious surface charging. The offset is typically smaller than 0.1−0.2 eV. Characterization of surface chemistry before catalysis was performed on the ambient pressure XPS system, since it acts as a high vacuum XPS while there is no gas introduced into the catalytic reactor. Au $4f_{7/2}$ was always collected immediately upon scanning Co 2p and O 1s under the exact same experimental conditions (same setting parameter of energy analyzer and same mixture of gases and sample temperature). All spectra are calibrated to their corresponding Au $4f_{7/2}$ which is 84.0 eV. Analyses of XPS peaks are performed with Casa program. Background subtraction influences the accuracy of the calculation of the peak area. For Co 2p (or O 1s) collected at different pressure or temperature, the same parameters including energy window, subtraction of background, line shape, and width are implemented to them, which makes comparison of O/Co ratio measurement at different temperatures valid.

Kinetics studies were performed in a fixed-bed flow reactor. Sample heating is well controlled by a PID controller. The flow rate of each gas was precisely controlled through their own flow meters. Water was introduced through a syringe pump with a precise control of flow rate (3.68 $\mu$L $min^{-1}$). The introduced water was heated to 110 °C and delivered to the catalytic reactor through 10% CO/Ar (aluminum cylinder, Airgas). The ratio of CO to $H_2O$ partial pressures is controlled through the flow rate of liquid water.

Surface chemistry characterization of catalysts during pretreatment or catalysis in Torr pressure range was performed on the in-house AP-XPS daily available in the Tao group.[40−42] Unlike in vacuum studies, reactant gases are introduced to flow through the catalyst at a certain temperature in the catalysis reactor of AP-XPS while data acquisition is going on. Gas flows through the reactor and exits through the exit port and an aperture that interfaces the gaseous environment in the catalytic reactor and vacuum environment of the pre-lens. Flow rate in the reactor was measured through a mass flow meter installed between each gas source and the entrance of the flow reaction cell. In this study, the flow rate of pure gas is in the range of 3−5 mL pure gas per minute (mL $min^{-1}$). The total pressure of the mixture gas of reactor is measured with a capacitance gauge installed at the entrance. The pressure at the exit is measured with another capacitance gauge. An average of the pressures at entrance and exit is defined to be the pressure above the catalyst in the catalytic reactor that was integrated with a monochromated Al K$\alpha$ X-ray source and a differential pumping stage. The catalyst is heated through heating the vacuum side of a sample stage using an e-beam heater installed in the vacuum section between the external wall of the catalytic reactor and the internal wall of the UHV chamber. The gaseous side is the internal wall of the reactor. The details are provided in ref 43.


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In situ X-ray absorption spectroscopy measurements were performed at the beamline X19A at the National Synchrotron Light Source, Brookhaven National Laboratory. The storage ring energy was 2.5 GeV, and the ring current was in the range of 110−300 mA. A double-crystal Si (111) monochromator was used to scan X-ray energy between 150 eV below and 583 eV above the Pt $L_2$ edge energy (13270 eV). Both $L_3$ and $L_2$ edges are appropriate for probing the d-electron density of Pt, directly affected by electronic charge transfer during the reaction. However, the $L_3$ edge is much closer in energy to the Co K-edge absorption edge. Hence, the total absorption is relatively high. Therefore, we collected the data at the Pt $L_2$ edge, which is further away from the Co K-edge energy during catalysis. The energy range was constrained by the onset of the Pt $L_1$ edge, but the resultant k-range available (0−12.1 $Å^{-1}$) was sufficiently large for quantitative EXAFS analysis. The samples were made by pressing the powders into circular pellets using a hydraulic press and then transferring them onto the sample holder of a Nashner−Adler in situ cell.[44,45] The X-ray absorption coefficient in metal Pt foil was measured in the reference mode for X-ray energy calibration and data alignment. Up to five consecutive scans were collected at each stage of the reaction to improve the signal-to-noise ratio.

EXAFS data processing and analysis were performed using the IFEFFIT package. EXAFS data modeling and analysis were performed using standard procedures.[46,47] The passive electron reduction factor was obtained to be 0.90 ± 0.08 from the fit to the Pt foil data and fixed to be 0.90 in the analysis of all Pt of Pt/$Co_3O_4$. Several parameters describing electronic properties, specifically, the correction to the original photoelectron energy, and local structural environment (coordination number ($N$), bond length ($R$), and mean squared disorder parameter ($\sigma^2$) of the nearest neighbors) around absorbing atoms were varied in the fit. Several models were compared for quantitative analysis of the EXAFS data. Theoretical EXAFS signals for Pt−O, Pt−Co, and Pt−Pt contributions were constructed using FEFF6 theory.

## 3. RESULTS AND DISCUSSION

**3.1. WGS on Nominal Catalyst $Co_3O_4$.** Figure 1 presents TEM images of pure cobalt oxide catalyst. The as-synthesized

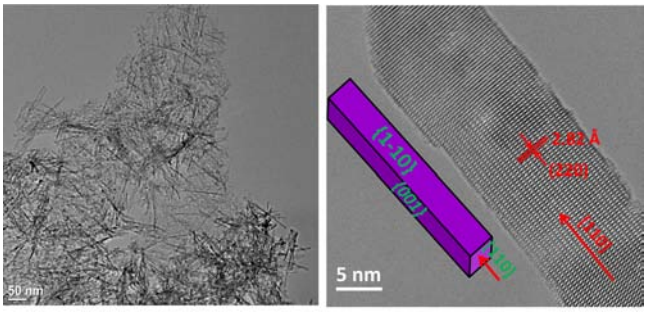


**Figure 1.** TEM image of $Co_3O_4$ nanorod catalyst. (a) Large scale. (b) High resolution TEM image.

$Co_3O_4$ exhibits a rod shape with a size of ~6 × ~6 × 100−200 nm. The measured interplanar distance is 2.82 Å along the extension direction of a nanorod (Figure 1b). Thus, the preferential exposed planes are (1−10) and (001). The two ends of a nanorod are (110). On (001) face, there is only $Co^{3+}$. There are two types of terminal faces (A and B) for (1−10). All Co atoms on the B-type surface are $Co^{3+}$, while $Co^{2+}$ and $Co^{3+}$ coexist on the type A surface of (1−10).

Kinetics studies of WGS on pure $Co_3O_4$ nanorods experienced a pretreatment at 200 °C in 5% $H_2$/Ar for 1 h were performed in a micro fixed-bed flow reactor with a flow rate of 150 mL $min^{-1}$ of mixture of reactants consisting of 3.3% CO and 3.3% $H_2O$. The temperature range of the kinetics studies was 180−240 °C. The highest conversion in this temperature regime was controlled to be lower than 15%. An Arrhenius plot (Figure 2) shows that the activation energy of WGS on pure cobalt oxide is 91.0 ± 10.5 kJ $mol^{-1}$.

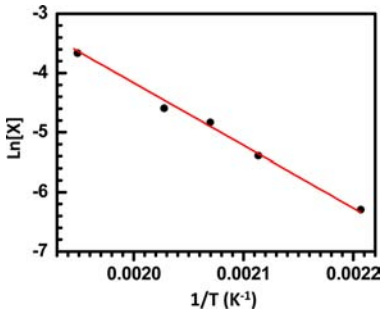


**Figure 2.** Kinetic studies of WGS on pure $Co_3O_4$ nanorod catalyst in the temperature range of 180−240 °C.

The surface chemistry of catalyst $Co_3O_4$ with pretreatment in 5% $H_2$/Ar at 200 °C and $Co_3O_4$ without any pretreatment during catalysis was examined using our in-house AP-XPS in the Torr pressure range of a gas mixture of pure CO and pure $H_2O$. Compared to the partial pressure of $H_2O$ in the mixture of reactants in a micro fixed-bed flow reactor of kinetic studies, ~25 Torr, the pressure of the reactant gases in a catalytic reactor of the AP-XPS system, a few Torr, is relatively low. The pressure of reactants contributes to the entropy and Gibbs free energy of the catalyst system, from a thermodynamic point of view. The pressure factor in Gibbs free energy is $kT \times \log P$. A difference in pressure of one magnitude results in a difference of only 0.03 eV in Gibbs free energy.[48] Typically, such a difference does not lead to an obvious difference in surface chemistry. Thus, we assume that the surface chemistry of the catalyst in a few Torrs of reactant gases is almost the same as that in a few tens of Torrs of reactant gases, although there could be a large difference between surface chemistry at a few Torrs and that in UHV ($10^{-10}$ Torr).[48]

Figure 3 shows the Co 2p and O 1s photoemission feature of $Co_3O_4$ nanorods, during pretreatment in $H_2$ at 200 °C, and during the followed catalysis with a flowing mixture of CO and $H_2O$ in the temperature range of 110−300 °C in an AP-XPS reactor. Co $2p_{3/2}$ and Co $2p_{1/2}$ of $Co_3O_4$ at room temperature appear at 779.7 and 794.7 eV, consistent with the data reported

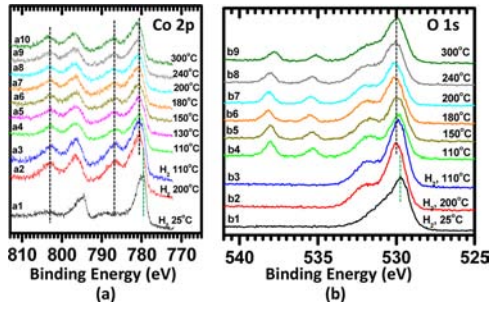


**Figure 3.** In situ AP-XPS studies of pure cobalt oxide catalyst in pretreatment of $H_2$ and the following catalysis in the temperature range of 110−300 °C in a mixture of CO and $H_2O$. The partial pressure ratio is 3:1. All spectra were collected when the gaseous environment existed around the catalyst.


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in the literature.[36,49] However, the photoemission features of both Co 2p and O 1s experience significant change upon $Co_3O_4$ pretreatment in $H_2$ at 200 °C; two very clear satellite peaks at 786.5 and 803.0 eV appeared after this pretreatment. The satellite photoemission features at 786.5 and 803.0 eV are characteristic features of $Co^{2+}$ and CoO since only $Co^{2+}$ ions on octahedral sites of rocksalt CoO could result in these unique photoemission features. $Co_3O_4$ does not have $Co^{2+}$ ions on its octahedral sites. Thus, the observation of satellite peaks at 786.5 and 803.0 eV (Figure 3a) clearly showed a phase transformation from $Co_3O_4$ to CoO. In addition, the main peaks of Co $2p_{3/2}$ and Co $2p_{1/2}$ in CoO upshift by 0.8 eV in contrast to $Co_3O_4$. This shift is due to the change of coordination environment of Co ions from $Co_3O_4$ to CoO. It is another evidence of the phase change during $H_2$ pretreated at 200 °C (Figure 3a2).

Upon pretreatment, the reactant gases were switched to a mixture of reactants CO and $H_2O$ (Figure 3, parts a3−a10). Photoemission features were collected while the catalyst functioned for WGS. The generation of products during data acquisition of AP-XPS was qualitatively analyzed with a quadruple mass spectrometer installed at lens 1 of the differential pumping system of AP-XPS.[40] It performs as real-time analysis of the gas leaking from the catalysis reactor of AP-XPS through the aperture on the catalytic reactor during catalysis. Interestingly, the CoO surface phase remains chemically stable in the mixture of CO and $H_2O$ even at a reaction temperature as low as 110 °C (Figure 3a4). In fact, a photoemission feature of Co 2p of CoO always remained throughout the entire temperature range of WGS, 110−300 °C upon $H_2$ pretreatment. O 1s photoemission features are presented in Figure 3b. Photoemission features of O 1s from oxygen atoms of gas phases of $H_2O$ and CO were clearly observed at ∼536 and ∼538 eV, respectively (Figure 3, parts b4−b9). They result from ionization of electrons on the subshell of oxygen atoms of gaseous molecules, which typically give a peak a few eV higher than that of the same subshell from atoms adsorbed on a catalyst surface.[48,50] It is noted that the observation of photoemission from molecules in the gas phase does not divert assignment of photoemission peaks of molecules adsorbed on the catalyst surface, due to the difference of a few eV in general. Alternatively, it provides solid evidence for the existence of gaseous reactants around the catalyst during data acquisition. Furthermore, the XPS spectra with gas phase peaks can be used to identify product molecules[51] if the conversion in catalytic reactor is high.

Quantitative analysis of photoemission features of Co 2p and O 1s allows us to calculate the O/Co atomic ratio of the surface region of catalysts (Figure 4). Although both CO and $H_2O$ of gas phases around the catalyst contribute to the O 1s photoemission, only O 1s photoemission intensity from surface of cobalt oxide (527−534 eV) was included in the calculation of O/Co atomic ratios. In addition, we assumed an O/Co ratio of $Co_3O_4$ at room temperature to be 1.33. It is understandable that there are oxygen vacancies on $Co_3O_4$ surface in a high temperature calcination during preparation. As $H_2O$ molecules in an ambient environment can dissociate on oxygen vacancies and thus OH groups are adsorbed at or fill these oxygen vacancies, the total number of oxygen atoms in the surface region of a $Co_3O_4$ with adsorbed OH groups at room temperature is approximately close to that of $Co_3O_4$ without oxygen vacancies. Thus, the O/Co ratio of $Co_3O_4$ before $H_2$ pretreatment can be considered to be 1.33. Upon this

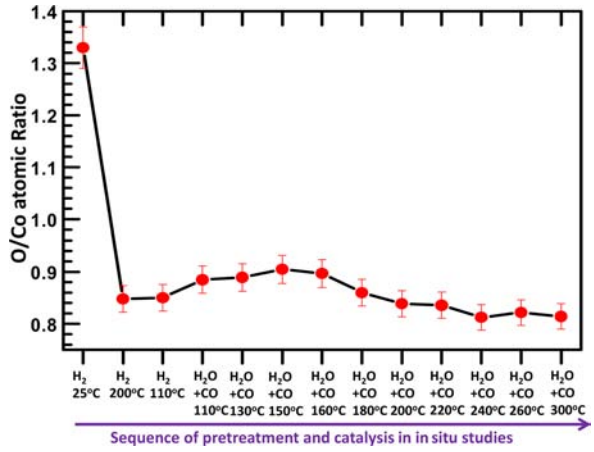


**Figure 4.** O/Co ratios measured during pretreatment and the following catalysis as a function of the sequential $H_2$ pretreatment and catalysis. The O/Co ratio of as-synthesized cobalt oxide ($Co_3O_4$) was defined to 1.33 which was used to calculate the O/Co ratios at other catalytic conditions.

assumption, a factor can be calculated by dividing the ratio of O 1s to Co 2p peak area with the stoichiometric ratio, 1.33. The atomic ratio of O/Co in pretreatment or during catalysis can be calculated by dividing the area ratio of O 1s to Co 2p at a catalytic condition with this factor calculated above. Figure 4 presents the O/Co atomic ratio as a function of pretreatment or catalytic conditions. Obviously, the O/Co atomic ratio is lower than 1 in $H_2$ pretreatment at 200 °C and during the following WGS catalysis in 110−300 °C. It shows a reduction of $Co_3O_4$ to CoO at 200 °C in $H_2$. The significant decrease of O/Co ratio is due to the change of surface phase from $Co_3O_4$ to CoO evidenced by the characteristic satellite peak of $Co^{2+}$ on octahedral sites of CoO (Figure 3). The O/Co ratio remains at ∼0.80−0.82 even during catalysis up to 300 °C. The in situ photoemission features of catalysts acquired during catalysis and the measured O/Co ratios in surface region clearly showed that the active phase of nominal catalyst $Co_3O_4$ nanorods is in fact nonstoichiometric cobalt monoxide, $CoO_{1-x}$. The easy formation of oxygen vacancies on $CoO_{1-x}$ could result from a larger Co−O bond length[37] and relatively weak bond strength in rocksalt CoO, in contrast to those of $Co_3O_4$.[35]

The as-synthesized $Co_3O_4$ *without* pretreatment in $H_2$ was studied by using AP-XPS during catalysis. Figure 5 shows the Co2p and O1s photoemission features at different catalysis temperature. Although cobalt oxide remains in its phase of $Co_3O_4$ at 100−140 °C in a mixture of reactant CO and $H_2O$, it is reduced to $CoO_{1-x}$ at 140−160 °C. This is evidenced by the

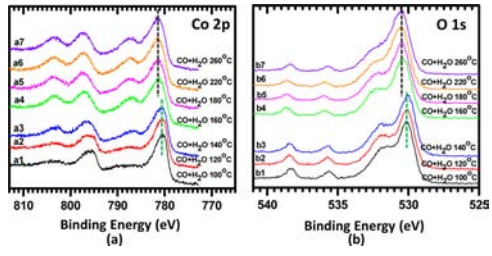


**Figure 5.** In situ AP-XPS studies of pure cobalt oxide catalyst during catalysis (there is no $H_2$ pretreatment) in the temperature range of 110−300 °C. The partial pressure ratio is 3:1. All spectra were collected when a catalyst is in a gaseous environment.


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appearance of satellite peaks in Figure 5, parts a4−a7. The formation of $CoO_{1-x}$ is also supported by the measured O/Co ratio at a temperature of 140−160 °C. As shown in Figure 6,

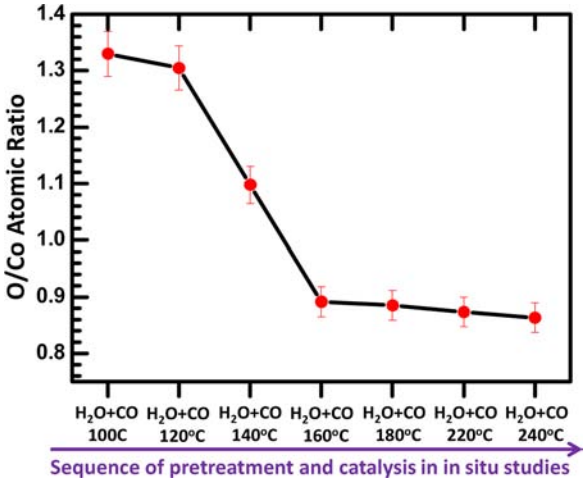


**Figure 6.** O/Co ratios of pure cobalt oxide catalyst measured during catalysis at different temperature (without $H_2$ pretreatment).

when temperature is higher than 140 °C, the O/Co ratio is decreased to 0.88 or so. Obviously, the surface phase during catalysis in temperature regime of 160−300 °C is $CoO_{1-x}$ which is the same as that of $Co_3O_4$ first pretreated in $H_2$ at 200 °C (Figures 3 and 4). Kinetics studies of $Co_3O_4$ (without pretreatment in $H_2$) in the temperature range of 180−240 °C show that its activation energy is very close to 91.0 kJ $mol^{-1}$ of the catalyst experienced a pretreatment in $H_2$ (Figure 2). The same surface chemistry and almost identical activation energy for catalyst *with a $H_2$ pretreatment* and *without a $H_2$ pretreatment* suggested that the active phase $CoO_{1-x}$ can be formed in a mixture of reactant gases (CO + $H_2O$) and products ($H_2$ + $CO_2$) during catalysis at certain reaction temperature even though there is no any $H_2$ pretreatment before WGS reaction.

The phase transformation of the $Co_3O_4$ catalyst under reaction conditions was studied with environmental TEM. As shown in Figure 7a, the bulk phase of $Co_3O_4$ in 0.3 Torr of reactant gases is transformed to CoO at 300 °C or so. In addition, the first peak of the O−K edge of $Co_3O_4$ (Figure 7d) observed at 200 °C disappears when the catalyst in the reactant gases was heated to 300 °C. The O−K edge resulting from the reactant gas was subtracted from the EELS spectra. The O−K edge starts to be weakened at 200 °C and disappears at 300 °C (Figure 7d). The EELS spectrum of the CoO in the reactant gases at 300 °C is consistent with the previous EELS spectrum of CoO under high vacuum.[52−54]

In summary, pure $Co_3O_4$ is restructured to nonstoichiometric $CoO_{1-x}$ in the reactants (CO and $H_2O$) of WGS. This was confirmed in our in situ studies of AP-XPS and E-TEM. $CoO_{1-x}$ is active for WGS, with an activation energy of 91.0 ± 10.5 kJ $mol^{-1}$ in the temperature range of 180−240 °C.

**3.2. WGS on Cobalt Oxide Anchoring Pt Atoms.** Pt/$Co_3O_4$ was synthesized through two steps. The first step is the synthesis of $Co_3O_4$ nanorods. After it is synthesized, Pt ions are anchored through deposition−precipitation, followed by a mild drying process and a subsequent calcination at 250 °C. TEM studies showed that the surface morphology is basically preserved, although roughening of the edge of the $Co_3O_4$ nanorods to some extent was definitely identified. The weight ratio of Pt to $Co_3O_4$ is 0.5%, equivalent to a Pt/Co atomic ratio of 0.2%. Since Pt ions were anchored on the surface of precrystallized $Co_3O_4$ nanorods through calcination at 250 °C, Pt ions are anchored on surface of $Co_3O_4$ nanorods. The atomic ratio (2.4%) of Pt to Co on the surface of a nanorod is actually much larger than the overall ratio (0.2%), since Pt atoms are anchored on $Co_3O_4$ already well crystallized. Calculations show that the low concentration of Pt atoms on a surface, $Pt_{surface}/Co_{surface}$ = 2.4% (see Supporting Information) certainly prevents them from aggregating to form Pt nanoclusters. STEM of the as-synthesized Pt/$Co_3O_4$ shows that the majority of Pt atoms are singly dispersed (Figure 8). This identification is consistent with the measured coordination number of Pt to Pt, zero, through analysis of EXAFS data of this catalyst to be described later in this work. As the Pt atom does not bond with another Pt atom in the as-synthesized 0.2% Pt/$Co_3O_4$, we call this as-synthesized catalyst, $Co_3O_4$ anchoring singly dispersed Pt atoms. It is written as $Pt_1/Co_3O_4$. In fact, EXAFS studies showed these Pt atoms in the as-synthetized catalyst bond solely to O atoms instead of Co.

Catalysis studies of $Pt_1/Co_3O_4$ were performed in a micro flow reactor. Kinetics measurements were performed in a kinetic control regime. Figure 9 is the Arrhenius plot in a temperature regime of 150−200 °C. On the basis of this plot activation energy of the catalyst is 50.1 ± 5.0 kJ $mol^{-1}$, much lower than the 91.0 ± 10.5 kJ $mol^{-1}$ of $CoO_{1-x}$ (Figure 2). More interestingly, kinetic measurement in the temperature

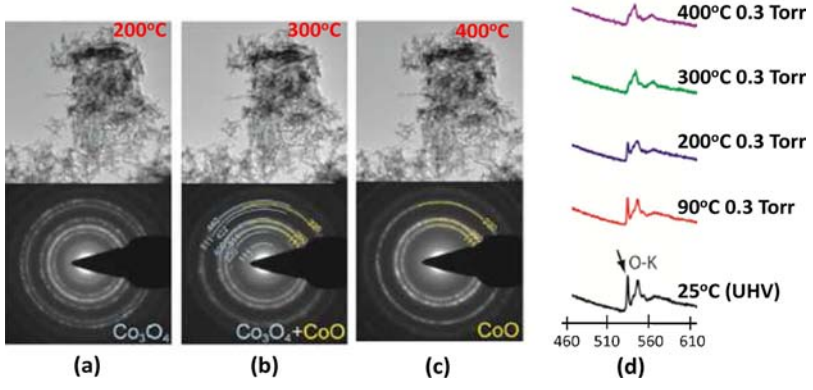


**Figure 7.** In situ TEM studies of $Co_3O_4$ nanorod catalysts at 0.3 Torr of reactant gas. (a)−(c): In situ diffraction patterns of $Co_3O_4$ nanorods in 0.3 Torr reactant gases at 200 °C, 300 °C, and 400 °C. (d) EELS spectra of $Co_3O_4$ nanorods at different temperatures in 0.3 Torr reactants.


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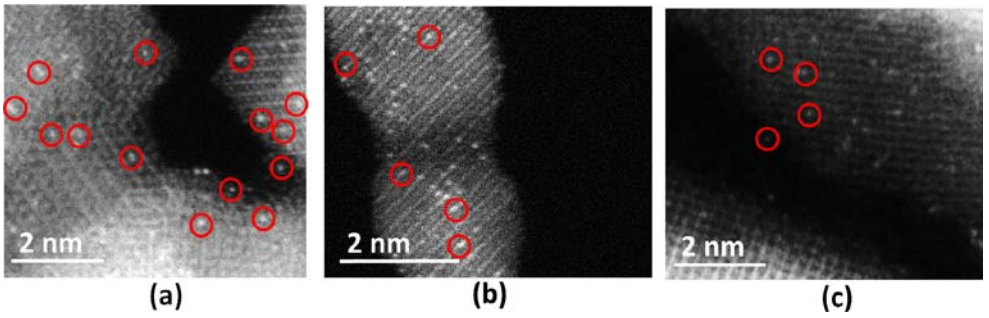


**Figure 8.** Images of aberration-corrected annular dark-field scanning transmission electron microscopy studies of $Co_3O_4$ with singly dispersed Pt atoms, $Pt_1/Co_3O_4$. Spots with high contrast (marked with red circles) are Pt atoms singly dispersed on $Co_3O_4$ nanorods. Images (a), (b), and (c) were collected at different areas randomly selected.

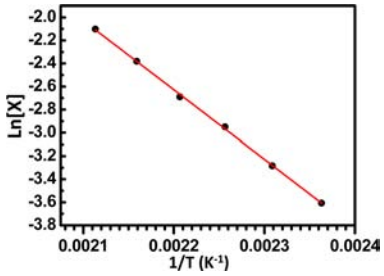


**Figure 9.** Kinetics studies of WGS on $Pt_1Co_n/Co_3O_4$ catalyst in the temperature range of 180−240 °C.

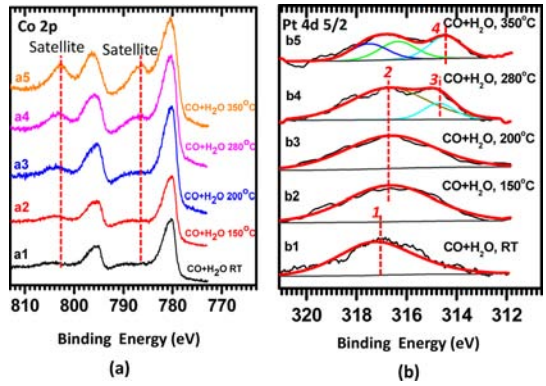


**Figure 11.** Photoemission features of Co 2p and Pt $4d_{5/2}$ of as-synthesized $Pt_1/Co_3O_4$ catalyst during catalysis at different temperatures. (a) Co 2p and (b) Pt $4d_{5/2}$. As Pt 4f overlaps photoemission features of Co 3p, Pt $4d_{5/2}$ was used to identify oxidation state and chemical environment of Pt anchored on $Co_3O_4$.

range of 300−350 °C exhibits quite different kinetics, as shown in Figure 10a. The activation energy in 300−350 °C is 24.8 ± 3.1 kJ $mol^{-1}$. The two quite different activation energies suggest different active phases in these two temperature ranges (150−200 °C versus 300−350 °C).

Figure 11 shows the photoemission features of Co 2p and Pt 4d5/2 of $Pt_1/Co_3O_4$ at room temperature and during catalysis at 150 °C, 200 °C, 280 °C, and 350 °C. Obviously, Co 2p remains the photoemission feature of $Co_3O_4$ at room temperature (Figure 11a1) and during catalysis at 150−200 °C (Figure 11, parts a2 and a3) since there are no any characteristic satellite peaks of $Co^{2+}$ of rocksalt CoO at 786.5 and 803.0 eV. The preservation of $Co_3O_4$ phase up to 200 °C during catalysis was further supported by the O/Co ratio of 1.10−1.15 at 150−200 °C. If the surface phase were $CoO_{1-x}$, then the O/Co ratio should have been 1 or lower. Thus, there is no phase transformation from $Co_3O_4$ to CoO in $Pt/Co_3O_4$ catalyst in the temperature range of 150−200 °C.

EXAFS studies were performed during catalysis in the temperature range of 25−300 °C. Figure 12 presents the Fourier transformed EXAFS data collected at the Pt $L_2$ edge at 25 and 200 °C during catalysis and their fitting analyses. Details of the fitting were described in the Experimental Section. The data and theoretical fit of metallic Pt foil are shown in Figure 12b. Figure 12c presents the fitting for data of the as-synthesized $Pt-Co_3O_4$ catalyst. This fitting suggests that Pt bonds predominantly with oxygen atoms instead of any Co atoms or Pt atoms. The measured coordination number of O atoms to a Pt atom is about 4.1 ± 1.9 (Table 1).

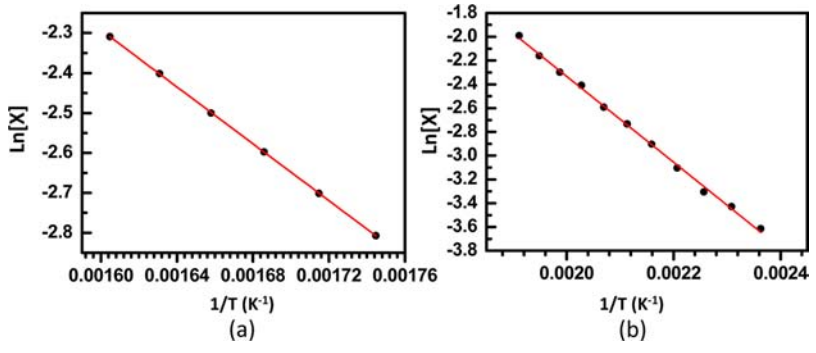


**Figure 10.** Kinetic studies of WGS on $Pt_mCo_{m'}/CoO_{1-x}$ catalyst in the temperature range of 300−350 °C (a) and 140−240 °C upon cooling it from 350 °C to 140 °C (b).


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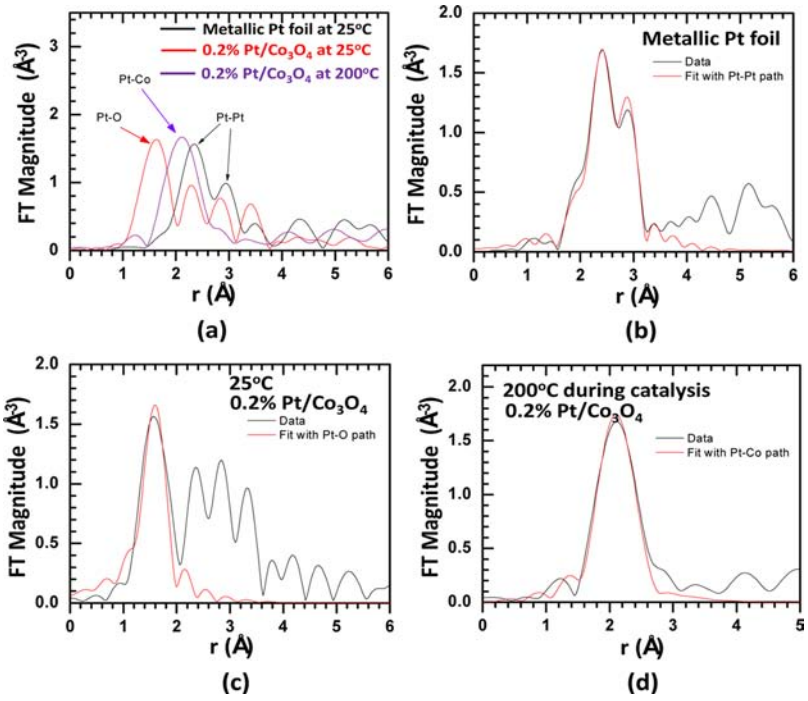


**Figure 12.** Catalytic in situ Pt $L_2$-edge EXAFS data and theoretical fits of $Pt_1/Co_3O_4$ at 25 °C and during catalysis at 200 °C. For comparison, data of metallic Pt foil were included as well. (a) Experimental data collected. (b) Fitting with Pt−Pt path of metallic Pt foil. (c) Fitting with Pt−O bond of as-synthesized $Pt_1/Co_3O_4$ at 25 °C. (d) Fitting with Pt−Co path of $Pt_1/Co_3O_4$ at 200 °C during catalysis.

**Table 1. Results of Quantitative Analyses for Pt−Pt, Pt−O, and Pt−Co Contributions to the EXAFS Data Obtained at 25 °C and during WGS at 200 °C**[a]

| sample | N(Pt−O) | N(Pt−Co) | R(Pt−O), Å | R(Pt−Co), Å |
|---|---|---|---|---|
| 25 °C, as prepared | 4.1 ± 1.9 | 0 | 2.01 ± 0.04 | |
| 200 °C, during WGS reaction | 0 | 7.1 ± 1.5 | | 2.54 ± 0.01 |

[a]Results of metallic Pt foil are shown as well for comparison. Only the coordination numbers and pair distances are shown. Standard deviations in the distances are shown in the SI.

EXAFS data at 200 °C during catalysis (Figure 12d) show that there is no presence of Pt−Pt or Pt−O bonds and the data are dominated by Pt−Co bonds. The quantitative analyses show that the coordination number of Co to Pt is 7.1 ± 1.5 (Table 1). The data indicate that Pt forms singly dispersed $PtCo_n$ nanoclusters on the oxide substrate during catalysis at 200 °C. Thus, the as-synthesized catalyst restructures to a new surface phase, $Pt_1Co_n$ ($n$ = 7.1 ± 1.5)/$Co_3O_4$ in which $Pt_1Co_n$ ($n$ = 7.1 ± 1.5) is singly distributed on $Co_3O_4$ surface.

Although the analysis of EXAFS data collected during catalysis at 200 °C demonstrate that Pt−Co dominates the experimental spectrum, such evidence is lacking for the catalyst during catalysis at 250 and 300 °C. Quantitative EXAFS analysis is not possible for the data of 250 and 300 °C due to the decreasing amplitude of EXAFS oscillations at these high temperature and, as a result, the poor signal-to-noise ratio. To examine the behavior of the catalyst at these high temperatures, 250 and 300 °C, we examined the X-ray absorption near edge structure (XANES) during catalysis at these temperatures, which is less affected by the catalysis temperature than the EXAFS data. Figure S6 of the SI presents the distinctive difference in the three regions (A, B, C) between XANES data at 200 °C corresponding to $Pt_1Co_n/Co_3O_4$ (Phase I) and those at 250 and 300 °C attributable to $Pt_mCo_{m'}/CoO_{1-x}$ (Phase II). The spectra at 250 and 300 °C (blue and yellow curves in Figure S6 of the SI) behave similarly to the metallic Pt foil (black curve in Figure S6 of the SI), while the spectrum at 200 °C (red curve in Figure S6 of the SI) shows distinct differences in these regions. This similarity of the XANES spectra during catalysis at 250 and 300 °C with Pt foil (black curve in Figure S8 of the SI) suggests that the sample at 250 and 300 °C contains Pt−Pt bonding contributions, in addition to Pt−Co.

The restructuring revealed in EXAFS studies is further supported by the AP-XPS data (Figure 11). To avoid overlap of Pt 4f with tail of Co 3p photoemission feature, Pt 4d5/2 was used to identify chemical state of Pt atoms during catalysis. The photoemission feature of Pd 4d5/2 has a wider distribution in terms of its full width at half-maximum (fwhm) due to its intrinsic short core-hole lifetime. The peak position of Pt 4d5/2 of the as-synthesized $Pt_1/Co_3O_4$ is 317.1 eV, which is consistent with Pt 4d5/2 of platinum oxide.[55,56] At 150 °C, the peak is broadened and down shifted by 0.7 to 316.4 eV during catalysis at 150 °C and remains the same photoemission feature at 200 °C during catalysis (Figure 11, parts b2 and b3). This down-shift results from a switch of binding environment of Pt atoms from Pt−O to Pt−Co based on EXAFS studies. Notably, the peak position of Pt $4d_{5/2}$ of $PtCo_n$ is still about 2 eV higher than metallic Pt,[55] resulting from the fact that each of the neighboring Co atoms of a Pt atom bonds with a few oxygen atoms (Figure 13b). This bonding likely makes Pt still positively charged to some extent. Thus, it still exhibits a binding energy higher than metallic Pt (Figure 11, parts b2 and b3).

These in situ studies showed that the active phase at 150−200 °C is $Pt_1Co_n$ nanoclusters embedded in the top layer of $Co_3O_4$. Figure 13, parts a and b, presents the structure of $Co_3O_4$ anchoring singly distributed $PtCo_n$ nanoclusters. The activation energy in the temperature range of 150−200 °C is


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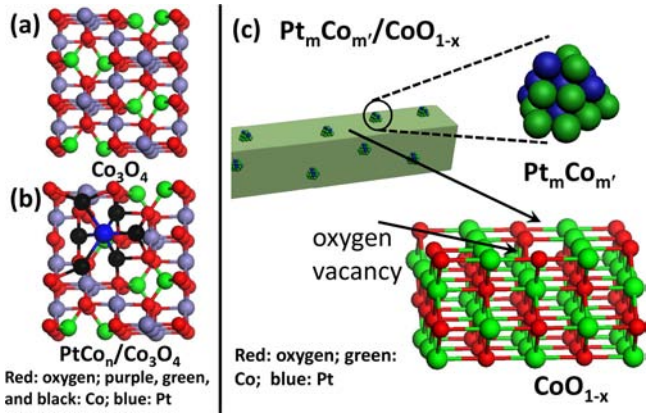


**Figure 13.** Structural models of surfaces of pure $Co_3O_4$ and active catalysts. (a) Top view of pure $Co_3O_4$. (b) Top view of $Pt_1Co_n/Co_3O_4$. (c) $Pt_mCo_{m'}/CoO_{1-x}$.

~50.1 ± 5.0 kJ mol$^{-1}$ (Figure 9). The TOF of $Pt_1Co_n/Co_3O_4$ at 200 °C based on the conversion measured in kinetics control regime is 0.40 $H_2$ molecules per Pt site per second. $Pt_1Co_n/Co_3O_4$ at 200 °C is ten times more active than $Pt/CeO_2$ at this temperature. This TOF (200 °C) is approximately equal to or higher than that of $Pt/CeO_2$ at 300 °C (Table 2, Figure 14). In addition, $Pt_1Co_n/Co_3O_4$ exhibits a high catalytic activity at 150 °C (TOF = 0.089). It suggests a very good catalytic performance of $Pt_1Co_n/Co_3O_4$ at low temperature such as 150 °C, although $Pt/CeO_2$ at 150 °C is not active. $Pt_mCo_{m'}/CoO_{1-x}$ formed through restructuring $Pt_1Co_n/Co_3O_4$ exhibits much higher TOF, 0.27 and 0.58 $H_2$ molecules per Pt site per second at 150 and 200 °C, respectively (Table 2), due to its low activation barrier of 29.6 kJ/mol.

As seen in Figure 11, parts a3–a5, the AP-XPS studies clearly showed a phase transition of $Co_3O_4$ of $Pt_1Co_n/Co_3O_4$ to $CoO_{1-x}$ in the temperature range of 200–300 °C. The main evidence is the appearance of a pair of satellite peaks of Co 2p of $Co^{2+}$ on the octahedral site of the oxygen atoms (Figure 11a5). The satellite peaks of Co 2p at 300 °C (Figure 11a5) are obvious. In addition, the O/Co ratio of catalysts at 300 °C is ~0.80 (not shown), further supporting a phase transformation from $Co_3O_4$ to $CoO_{1-x}$ in the temperature range of 250–300 °C.

The change at a temperature of 280 °C reflects the chemical state of the Pt ions. An additional photoemission of the Pd 4d5/2 feature of the doped catalyst at a temperature of 280 °C (Figure 11b4) exhibits a broad peak centered at a low binding energy at ~315.8 eV. It showed an obvious change in the chemical states of the Pt atoms in the temperature range of 250–300 °C. Since $Co_3O_4$ of the catalyst is reduced to $CoO_{0.8}$ in the temperature range of 200–300 °C (Figure 11, parts a3–a5), we would consider that new Pt–Co nanoclusters are formed in the phase transformation from $Co_3O_4$ to CoO. The binding energy of Pt 4d5/2 at 280 °C (peak 2) is obviously down-shifted by 0.5 eV in contrast to peak 1 at room temperature. Notably, an obvious low-energy shoulder at 314.4 eV (peaks 3 and 4 in Figure 11, parts b4 and b5, respectively) appeared at 280 and 350 °C in contrast to those of 200 °C in the first annealing cycle (Figure 11b3). The position of the low-energy shoulder is consistent with the Pt 4d5/2 of Pt metal found in the literature.[64,65] Since the contribution from metallic Pt at 314.4 eV was clearly identified and there is still a large contribution at 316.4 eV attributable to Pt–Co, we would

**Table 2. List of Turnover-Frequency of Catalysts Reported in This Work and Pt–$CeO_2$ and Pt–$TiO_2$ in the Literature**

| temperature (°C) | $CoO_{1-x}$ | $Pt_1Co_n/Co_3O_4$ | $Pt_mCo_{m'}/CoO_{1-x}$ | $Pt/CeO_2$ | | | $Pt/TiO_2$ | | |
|---|---|---|---|---|---|---|---|---|---|
| 150 | | 0.089 | 0.27[a] | | | | 0.078 (ref 59) | 0.093 (ref 57) | 0.093 (ref 58) |
| 200 | 0.000261 | 0.40 | 0.58[a] | 0.052 (ref 57) | 0.037 (ref 58) | | 0.0156 (ref 59) | 0.50 (ref 57) | 0.28 (ref 58) |
| 250 | 0.00147 | | 0.84[a] | 0.44 (ref 57) | 0.21 (ref 58) | 0.08 (ref 58) | 0.039 (ref 59) | | 0.37 (ref 58) |
| 300 | | | 2.37[a] | 0.2 (ref 60) | 0.39 (ref 58) | 0.27 (ref 58) | 0.086 (ref 59) | | |
| 350 | | | 3.90[a] | | | | | | |

[a]TOF of $Pt_mCo_{m'}/CoO_{1-x}$ when all Pt atoms are assumed to be active sites.


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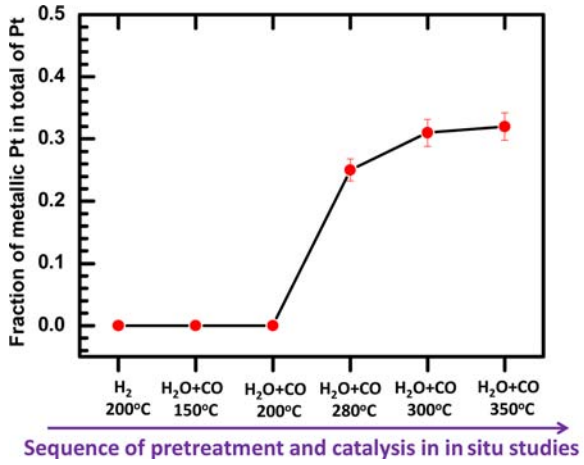


**Figure 14.** Atomic fraction of Pt of Pt 3d peak with a binding energy at 314.2 eV based on a consistent deconvolution of Pt 3d photoemission features of of nominal catalyst $Pt/Co_3O_4$ during catalysis. The active phases of the catalysts in the temperature range of 150−200 °C and 300−350 °C are $PtCo_n/Co_3O_4$ and $Pt_mCo_{m'}/CoO_{1-x}$, respectively.

suggest that bimetallic nanoclsuters $Pt_mCo_{m'}$ were formed along the restructuring of $Co_3O_4$ substrate to $CoO_{1-x}$ in the mixture of reactant gases. Our in situ AP-XPS studies and the deconvolution of spectra of $Pt_mCo_{m'}/CoO_{1-x}$ obtained at 350 °C (Figure 11b5) showed that the Pt 4d5/2 photoemission feature of $Pt_mCo_{m'}/CoO_{1-x}$ is contributed from Pt−O at 317.5 eV,[56] Pt−Co−O at 316.4 eV, and Pt−Pt at 314.4 eV,[55] respectively. The three features contribute ∼36%, ∼32%, and ∼32% of the intensity of Pt 4d5/2, respectively (Figure 11b5). From these analyses, approximately 32% of atoms of a $Pt_mCo_{m'}$ nanocluster are Co atoms, on average.

In each of such $Pt_mCo_{m'}$ nanoclusters, some Pt atoms bond with Pt atoms and the other with Co and O atoms. As $Co_3O_4$ is reduced to $CoO_{1-x}$ at 300 °C, we would term the active phase to be $Pt_mCo_{m'}/CoO_{1-x}$. Figure 13c presents the structural scheme of $Pt_mCo_{m'}/CoO_{1-x}$. Compared to pure $CoO_{1-x}$ formed from pure $Co_3O_4$ (Figure 2), the activation energy on $Pt_mCo_{m'}/CoO_{1-x}$ (Figure 10) is much lower, which clearly suggests the significance of $Pt_mCo_{m'}$ nanoclusters (Table 3).

**Table 3. Activation Energies of $Co_3O_4$ (Nominal Catalyst) and $Pt_1/Co_3O_4$ (Nominal Catalyst), and $Pt/CeO_2$ and $Pt/TiO_2$**

| nominal catalyst | surface of active catalyst | activation energy (kJ/mol) | temperature range of kinetic studies (°C) | references |
|---|---|---|---|---|
| $Co_3O_4$ | $CoO_{1-x}$ | 91.0 | 180−280 | this work |
| 0.2%Pt/$Co_3O_4$ | $PtCo_n/Co_3O_4$ | 49.9 | 150−200 | this work |
| 0.2%Pt/$Co_3O_4$ | $Pt_mCo_{m'}/CoO_{1-x}$ | 24.8 | 300−350 | this work |
| | | 29.6 | 140−240 | this work |
| Pt−$CeO_2$ | $Pt/CeO_{2-x}$ | 46.1 | 150−350 | ref 61 |
| | | 91 ± 5 | 150−400 | ref 60 |
| | | 100.48 | 200−250 | ref 57 |
| | | 60 ± 2 | 175−250 | ref 62 |
| Pt−$TiO_2$ | $Pt/TiO_{2-x}$ | 45.2 | 200−420 | ref 59 |
| | | 59 ± 3 | 150−400 | ref 60 |
| | | 64.9 | 180−280 | ref 57 |
| | | 65.7 | 180−280 | ref 63 |

To examine a potential influence of gas composition on kinetic studies and surface chemistry of catalysts, measurement of the $E_a$ of as-synthesized $Pt_1/Co_3O_4$ catalyst in the two different temperature ranges of 150−200 °C and 300−350 °C were performed in a mixture of reactants CO and $H_2O$ with a ratio of 1:3 instead of the 3:1 ratio used in Figures 9 and 10. In the temperature range of 150−200 °C, the measured $E_a$ of catalysts in the reactions of CO and $H_2O$, with a ratio of 1:3, is close to the 50.1 ± 5.0 kJ $mol^{-1}$ value measured in the mixture of CO and $H_2O$, with a ratio of 3:1. In the temperature range of 300−350 °C, it is 29.6 ± 4.0 kJ $mol^{-1}$, similar to the 24.8 ± 3.1 kJ $mol^{-1}$ value found for the CO:$H_2O$ ratio of 3:1. These studies suggest that the gas composition of reactants does not obviously vary the kinetics and surface chemistry of $Pt_1Co_n/Co_3O_4$ and $Pt_mCo_{m'}/CoO_{1-x}$.

Table 3 lists the activation energies of $CoO_{1-x}$, $PtCo_n/Co_3O_4$, $Pt_mCo_{m'}/CoO_{1-x}$ measured here, and $Pt/CeO_2$ and $Pt/TiO_2$ reported in the literature. $Pt_mCo_{m'}/CoO_{1-x}$ has the lowest activation energy. The turnover frequency of generation of $H_2$ on the three catalysts at different temperatures was calculated. They are listed in Table 2. When compared to the TOF of $H_2$ generation on $Pt/CeO_2$ and $Pt/TiO_2$, $Pt_mCo_{m'}/CoO_{1-x}$ exhibits a higher TOF (Table 2). For example, the TOF at 350 °C $Pt_mCo_{m'}/CoO_{1-x}$ is 35 times higher than that of $Pt/TiO_2$ at this temperature. Notably, the $Pt_mCo_{m'}/CoO_{1-x}$ phase exhibits a high catalytic activity in the low-temperature range of 140−240 °C, upon being cooled to 140 °C from 350 °C. Figure 10b is the Arrhenius plot in this temperature regime. The activation energy calculated from this Arrhenius plot is 29.6 kJ/mol. It is in good agreement with the activation energy measured at the high temperatures of 300−350 °C. The higher catalytic activity of $Pt_mCo_{m'}/CoO_{1-x}$ in contrast to $Pt/CeO_2$ is likely partially contributed from both the difference in the metal components ($Pt_mCo_{m'}/CoO_{1-x}$ nanoclusters versus Pt nanoparticles) and the difference in the reducible oxides (nonstoichiometric $CoO_{1-x}$ versus $CeO_2$). Oxygen vacancies of reducible oxides such as $CeO_2$ and $TiO_2$ are considered to be the sites of adsorption with a following dissociation of $H_2O$.[7] Similarly, we consider oxygen vacancies of $CoO_{1-x}$ on $Pt_mCo_{m'}/CoO_{1-x}$ to be the sites that disassociate $H_2O$. Different from oxygen vacancies in $CeO_2$ and $TiO_2$, an oxygen vacancy on $CoO_{1-x}$ could retain a pair of electrons. It is similar to an oxygen vacancy of MgO.[66−68] However, the Ce or Ti atom of an oxygen vacancy on $CeO_{2-x}$ and $TiO_{2-x}$ is in fact in a reduced valence state, $Ce^{3+}$ and $Ti^{3+}$. It seems that an oxygen vacancy on the surface of $CoO_{1-x}$ has a different electronic structure compared to those on $CeO_{2-x}$ and $TiO_{2-x}$. We expect that oxygen vacancies on the $CoO_{1-x}$ surface play a role similar to that of the MgO surface with regard to adsorption and dissociation of $H_2O$. Both experimental and theoretical studies have shown that dissociation of $H_2O$ on an MgO surface is performed by oxygen vacancies.[67,68] Computational studies on the electronic structures of the oxygen vacancies of $CoO_{1-x}$ and its adsorption of $H_2O$ would certainly help in our understanding of the role of $CoO_{1-x}$ in $Pt_mCo_{m'}/CoO_{1-x}$.

## 4. CONCLUSIONS

We reported three different WGS catalysts, $CoO_{1-x}$, $Pt_1Co_n/Co_3O_4$, and $Pt_mCo_{m'}/CoO_{1-x}$. Their active surfaces during catalysis were identified with different in situ surface analytical techniques: AP-XPS, EXAFS, and E-TEM. Their kinetics were studied in the kinetic control regime. $Pt_mCo_{m'}/CoO_{1-x}$ exhibits the lowest activation energy in contrast to pure $CoO_{1-x}$ and


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$Pt_1Co_n/Co_3O_4$, probably due to the synergic effect of the nanoclusters $Pt_mCo_{m'}$ and oxygen vacancies of $CoO_{1-x}$. Oxygen vacancies of $CoO_{1-x}$ could play a different role in the adsorption and dissociation of $H_2O$ molecules in contrast to that of $CeO_{2-x}$ and $TiO_{2-x}$. The different catalytic performances of $CoO_{1-x}$, $Pt_1Co_n/Co_3O_4$, and $Pt_mCo_{m'}/CoO_{1-x}$, restructured from $Co_3O_4$ and $Pt_1/Co_3O_4$, suggested a method of tuning catalytic performance and developing catalysts through restructuring the oxide catalyst in the gas phases.

## ■ ASSOCIATED CONTENT

### Supporting Information

Synthesis of catalysts; calculation of the atomic ratio of Pt to Co atoms on topmost surface of a 0.2% $Pt_1/Co_3O_4$ nanorod; standard deviation in analysis of Pt−O, Pt−Co, and Pt−Pt bonds from EXAFS data; ambient pressure X-ray photoelectron spectroscopy and in situ studies of surface chemistry of catalysts during catalysis and under reaction conditions; analysis of X-ray absorption near edge structure of catlaysts during catalysis; and ADF-STEM images of $Pt_mCo_{m'}$ nanoclusters formed during catalysis at high temperatures. This material is available free of charge via the Internet at http://pubs.acs.org.

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### Notes

The authors declare no competing financial interest.

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